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Adsorption of Ni (II) from aqueous solution by fly Ash

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Abstract

Fly ash adsorbent was used for the removal of nickel ions from aqueous solution of Shahdol. The solution of Nickel was prepared of 100 ppm & Analyzed by AAS. Sorption of metal ion has been studied as function of contact time, Temperature, PH of the solution and metal ion concentration. These factors have Remarkable positive effect on sorption Process.

The Adsorption data of fly Ash at different initial concentration was fitted to freundlich & Langmuir adsorption isotherms and monolayer sorption capacity determined was 94.5 (Ph 5.0 Temperature 27^oc) Thermodynamics parameter indicates that the sorption is Exothermic, spontaneous with a greater affinity of metal species for the adsorbent.

Keywords: sorption, fly ash, activated carbon, AAS

Introduction

We study the fly ash as an adsorbent for the removal of Heavy metals from aqueous solution. Fly Ash is a powdered material produced by the combustion of pulverized coal in thermal Power Plants ^[1].

A Number of methods are available for the Removal of metals ions from aqueous solution, Preparation of fly ash adsorbent sample, studied contact time, temperature ph of the solution and metal ion concentration. Heavy metals found in fly Ash are Toxic in Nature ^[2, 3].

Fly ash defined in cement and concrete terminology as "The finely divided Residue resulting from the combustion of granular or powdered coal, which is transported from the hearth through the stoker by flue gases". Fly ash is a by-product of coal-fired electric generating plants.

Fly ash is a finely divided residue resulting from the combustion of powdered coal lignite and collected from the flue gas of pulverized fuel fired boilers with the help of electrostatic precipitators. It is generally grey in colour, abrasive, refractory, generally acidic in nature. It has a specific surface area which varies between 2500 and 7000 sq. m and possesses pozzolanic characteristics. Particle size of fly ash ranges from as high as 120 to as low as less than 5 microns, it also contains particles of unburnt carbon soot.

Fly ash is a waste material generated from electric power plants and approximately 500 million tonnes of fly ash is discharged per year throughout the world. Because fly ash has pozzolanic properties after reacting with lime ^[4] about 20 % of fly ash is used as building materials. However, the remaining fly ash disposed in landfills still causes an increasing threat to the environment due to its fine structure and toxic elements as one of the economically viable solutions, the utilization of fly ash as inexpensive adsorbents has not also been widely attempted far. Blue gas cleaning ^[5, 7] and removal of toxic metals ^[8-13] and organisms ^[14] from waste waters. However, in cases, the fly ash still exhibits low adsorption capacity.

Experimental

Preparation of fly ash adsorbent sample for our study: a stock solution of Nickel (II) can be made of either NiSO₄ · 7H₂O as Nickel chloride NiCl₂ · 6H₂O. We made 1000 ppm solution of NiSO₄ · 7H₂O in 100 ml water.

All reagents are AR or GR grade. 100 ml of metal solution is taken with 0.5 gm of fly ash. The solution is shaken for 100 rpm after about 30 minutes. The supernatant was withdrawn from the shaker, centrifuged and the supernatant solution was analyzed for residual metals by AAS.

Result and Discussion

Studies of various factors such as contact time, pH, adsorbent dose, metal ion concentration, and temperature on the adsorption can be given in the following way. The results obtained from

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AAS study is shown in table 1 and it is evident that the adsorption of Ni (II) is maximum at this concentration and at Ph 5.0 the contact time was 60 min.

Table 1: Removal of Ni (II) by fly ash temperature 303 k PH 5.0 Contact time 60 min

| S.No. | Weight of Adsorbent gm/100ml | Time (min) | Adsorbed | % Removal of metal ion |
|-------|------------------------------|------------|----------|------------------------|
| 1 | 0.5 | 15 | 179 | 17.9 |
| 2 | 0.5 | 30 | 278 | 27.8 |
| 3 | 0.5 | 45 | 462 | 46.2 |
| 4 | 0.5 | 60 | 930 | 93.0 |
| 5 | 0.5 | 75 | 935 | 93.5 |
| 6 | 0.5 | 90 | 946 | 94.6 |
| 7 | 0.5 | 105 | 959 | 95.9 |

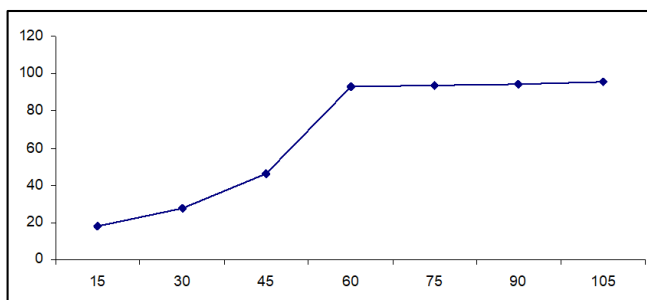


Fig 1: Effect of Contact time on adsorption of Ni (II) 303k on fly ash

The dependence of sorption of Ni (II) on contact time was determined by batch techniques at different time intervals of 15 mins, 30 mins, 45 min, 60 min, 90 min, 105 min, at 303 k maximum adsorption was achieved at 105 mins 95.9%.

The removal of metal ions from aqueous solution by adsorption is highly dependent on the pH of the solution which affects the surface charge of the adsorbent, the degree of ionization and speciation of the adsorbate.

Table-2 & Figure-2 illustrate the influence of pH on adsorption and indicate that the pH of the solution plays a vital role in any adsorption process. The removal of these methods increased with increases in pH and reached a shoulder-like maximum followed by a sharp increase in removed amount to 99% over the pH range 5 to 7.

Table 2: Percentage adsorption of Ni (II) by fly ash (Effect of PH) Temp. 303 K Adsorbent weight 0.5 gm contact time 60min

| S.N. | PH | Removed Amount of Ni(II) in ppm | Removed % Ni(II) |
|------|----|---------------------------------|------------------|
| 1 | 3 | 245 | 24.5 |
| 2 | 4 | 655 | 65.5 |
| 3 | 5 | 930 | 93.0 |
| 4 | 6 | 965 | 96.5 |
| 5 | 7 | 970 | 97.0 |

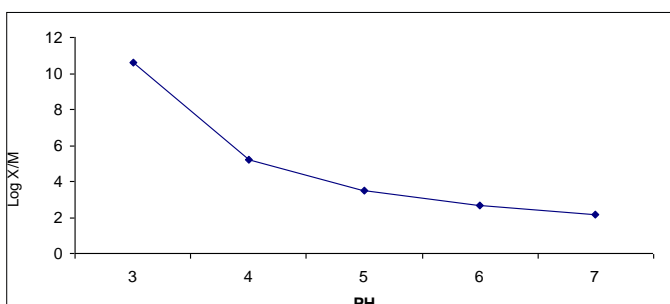


Fig 2: Effect of PH on adsorption of Ni (II) At 303 Fly Ash

The effect of adsorbent dose was studied by varying the amount of adsorbent dose (0.01, 0.02, 0.03, 0.04, 0.05, 0.06, 0.07, 0.08) and performing the studies at pH 5.0. The data obtained are depicted in table-3 and figure-3.

The data obtained in the study indicated that the amount of Ni (II) adsorbed on fly ash significantly increased with increase in the adsorbent dose.

Similarly, the removed percentage of Ni (II) with the increasing adsorbent dose rose from 62.0% to 94.0% so like the other factors of adsorption dose of adsorbent also plays a vital role in the removal of metal ion from the solution.

The higher dose of adsorbent due to an increase in surface area would have caused the availability of more number of adsorption sites, resulting in higher metal removal. At the adsorbent dose of 0.08 gm maximum at 94.0% initial was obtained.

Table 3: Effect of adsorbent dose on adsorption of Ni (II) by fly Ash Temperature 303 k Ph 5.0 Contact time 60 min

| S. No. | Adsorbent dose gm/ 100ml | Removed amount of Ni (II) in ppm | Removed % Ni (II) |
|--------|--------------------------|----------------------------------|-------------------|
| 1 | 0.01 | 620 | 62.0 |
| 2 | 0.02 | 850 | 85.0 |
| 3 | 0.03 | 900 | 90.0 |
| 4 | 0.04 | 920 | 92.0 |
| 5 | 0.05 | 930 | 93.0 |
| 6 | 0.06 | 936 | 93.6 |
| 7 | 0.07 | 940 | 94.0 |
| 8 | 0.08 | 940 | 94.0 |

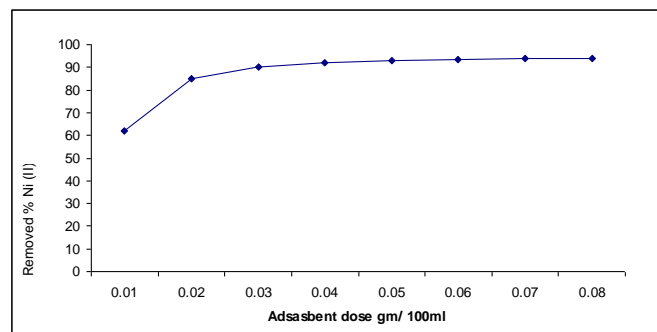


Fig 3: Effect of Adsorbent dose on adsorption of Ni (II) at 303 k on Fly ash

The effect of initial concentration of metal ions on the sorption potential of adsorbent fly ash at the temperature 303 k was investigated at pH 5.0 and the adsorption data of adsorbent at different initial concentrations of Ni (II) is shown in table-4. The results so obtained were fitted to the line as the Langmuir and Freundlich adsorption isotherms. The adsorption increases with the metal ion concentration increase as shown in.

Table 4: Table adsorption of Ni (II) on fly ash with varying metal concentration temperature 303 k Adsorbent dose 0.5gm Ph 5.0 contact time 60 min

| Initial Con. mg/L | C_e | X | X/M | $\log C_e$ | $\log X/M$ | $\frac{1}{C_e}$ | $\frac{1}{x/m}$ |
|-------------------|-------|--------|-------|------------|------------|-----------------|-----------------|
| 50 | 1.10 | 47.12 | 0.094 | 0.041 | -1.026 | 0.909 | 10.63 |
| 100 | 2.10 | 96.71 | 0.193 | 0.322 | -0.714 | 0.476 | 5.18 |
| 150 | 5.13 | 143.12 | 0.286 | 0.710 | -0.543 | 0.194 | 3.49 |
| 200 | 9.98 | 188.64 | 0.377 | 0.994 | -0.423 | 0.101 | 2.65 |
| 250 | 13.12 | 233.72 | 0.467 | 0.117 | -0.330 | 0.076 | 2.14 |

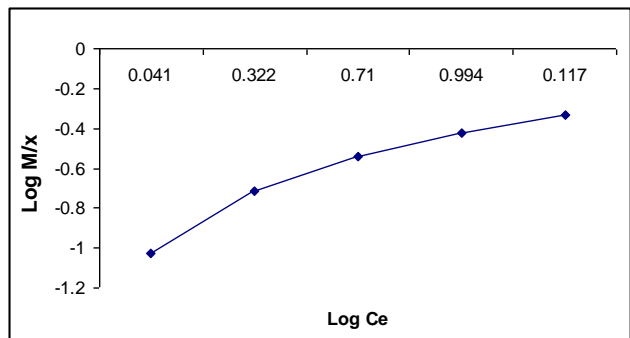


Fig 4: Freundlich adsorption isotherm of Ni (II) at 303 k on Fly Ash

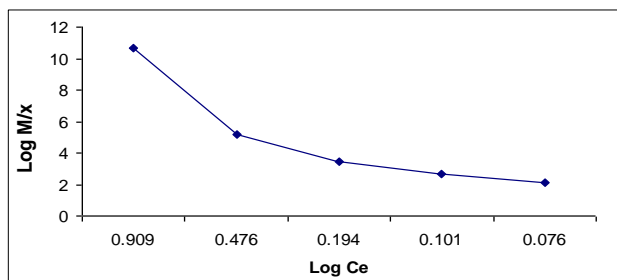


Fig 5: Langmuir adsorption of Ni (II) at 303 k on Fly Ash

The Freundlich & Langmuir model has been applied to the experimental data & Result shows that both models are fit to the study. The linear plots of $1/x$ versus $1/C_e$ clearly indicate monolayer coverage of adsorbate at the outer surface of the sorbent.

The adsorption data obtained with the adsorbent correlate will with the Freundlich & Langmuir adsorption models. Freundlich Content form adsorption data are given in the

table-5 the value of K increased as temperature increased indicating that adsorption increases or temperature increases. The value r comes between 1 to 10 represents beneficial adsorption.

Table 5: Value of Freundlich Constants for pb (II)

| Metal Ion | Log | | 1/n | | r(Corr. coefficient) | |
|-----------|---------|--------|-------|-------|----------------------|-------|
| | 303k | 313k | 303k | 313k | 303k | 313k |
| Ni (II) | -0.9738 | -0.986 | 0.556 | 0.595 | 0.984 | 0.980 |

Values of Freundlich & Langmuir constants, RL Values & Thermo dynamic parameters are calculated and shown in the table 6 and 7 from the data shown in table 6 it is evident that the exothermic nature of the Adsorption is indicated by a decrease q_0 with rise in temperature the result shown in table 6 also indicate ΔG^0 values are negative which means that the reactions spontaneous the values of ΔG^0 generally increased with temperature pointing towards sharp spontaneity of the reaction and sharp change in affinity of metal ions by fly Ash. The Negative values of ΔH^0 Suggested that the adsorption was exothermic also negative values of ΔH^0 Suggest that the adsorption was energetically stable

As indicate table ΔS^0 values for the adsorption process are positive. Positive entropy of adsorption also reflects the affinity of adsorbent material for Ni (II).

The Positive value of Entropy also suggests a high degree of disorderliness at the solid solution interface during the adsorption of metal ions fly Ash.

The value of R_L indicates the shape of the isotherm to be either unworkable ($R_L > 1$) linear ($R_L = 1$) favorable ($0 < R_L < 1$) as irreversible ($R_L = 0$)

This study shows that the shape of the iso thermo is favorable ie. R_L values ($0 < R_L < 1$).

Table 6: Values of langmuir constants and thermodynamics parameter

| Metal Ion | q value related to the equilibrium constant (Lmole ⁻¹) | | b (ln g ⁻¹) | | ΔG^0 K. Cal mole ⁻¹ | | Mean ΔH^0 K. Cal mole ⁻¹ | Mean ΔS^0 K. Cal mole ⁻¹ |
|-----------|--|--------|-------------------------|-------|--|---------|---|---|
| | 303K | 313K | 303K | 313k | 303k | 313k | | |
| Ni(II) | 1.6311 | 1.3812 | 8.921 | 9.762 | -0.3219 | -0.3559 | -0.00029 | 0.00109 |

Table 7: Equilibrium parameters R_L calculated from langmuir adsorption isotherm

| Metal Ion Concentration (mg/L) | Pb (II) | |
|--------------------------------|---------|---------|
| | 303k | 313k |
| 50 | 0.00223 | 0.00204 |
| 100 | 0.00111 | 0.00102 |
| 150 | 0.00074 | 0.00068 |
| 200 | 0.00056 | 0.00051 |
| 250 | 0.00044 | 0.00040 |

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